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# Pyrolysis behaviour study of date palm biomass in Algerian oasis using thermogravimetric analysis.Deglet Nour cultivar case

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*Abstract*— The objective of this work is the study of the thermal behavior, under an oxidative atmosphere of the phoenicicole biomass main constituents related to the dominant cultivar, Deglet Nour (DN). Thermogravimetric analysis (TGA) is the approach used to study the pyrolysis behavior of this lignocellulosic biomass, the determination of the kinetic constant (activation energy, order of the reaction, pre-exponential factor), the description of different thermal profile. The statistical method used for the examination of the TGA data are the analysis of variance ANOVA and principal component analysis PCA.

The results show that pyrolysis process could be an interesting alternative energy recovery for the phoenicicole biomass. This is explained by the low activation energy which is estimated on the average at 28.78 k J/mol. For the whole studied biomass, kinetic, thermal and chemical parameters are advantageous in comparison with conventional solids biofuels. An exception was observed for Lif part which is unsuitable for pyrolysis process because of its thermal stability.

Keywords-Phoenicicole biomass; Thermogravimetric; Kinetics; Pyrolysis ; Classification

#### I. INTRODUCTION

Biomass is a sustainable alternative to the numerous planetary preoccupations related to climate change in general and greenhouse gases in particular [1]. It has many advantages that make it competitive or even preferred over other renewable energy i.e.: a very substantial deposit (especially lignocellulosic resources), a zero carbon footprint, a waste recycling...[2] In the Oasis context, the date palm (*Phoenix dactylifera L.*) could be considered an attractive and sustainable energy source since it offers many advantages (biochemical, ecological, socio-economic, environmental ...) [3-10]. The thermal behavior study of this biomass is an essential step for an initial evaluation of its energy quality [1, 7].

In recent years, many technologies have been the subject of studies on the potential energy uses of biomass. This is precisely the case of pyrolysis which is very promising in this field. The study of this latter, appears to be necessary and a priority because it is a precursor process for all chemical thermoconversions (Combustion, gasification, liquefaction ...) [11]. However, the biomass pyrolysis is a very complex process, governed by a series of reaction which kinetics is influenced by multiple factors: physical type of biomass, heat transfer and mass, operating conditions (Heating rate, gas flow ...). At an analytical level, we add to these factors the analysis methodology and the equipment used[12].

Thermogravimetric analysis (TGA) is one of the most commonly used analytical techniques for the study of the biomass thermal behavior under pyrolysis. It is a simple and rapid method based on the determination of the weight change depending on the temperature; and that essentially considers the weight, temperature and time. The interpretation and exploitation of the curves obtained require the drawing of the derivative thermogravimetric DTG. The determination of kinetic parameters responsible for the prediction of the Arrhenius model. However, the low heating rate (important run time) and the need to use small amounts (representability problem results) are, limitations to this technique [1, 9, 13-15].

The choice of phoenicicole biomass for this study is based on several reasons. The first one is its chemical quality compatible with that of conventional biofuels [6, 7]. The second reason is the scarcity of studies in the chosen thermal conversion field [6-9]. The third reason is the importance of biomass deposit in the Algerian oasis especially cultivar selected for this study. This last one represents 40% of Algerian phoenicicole park and generates significant amounts of residues (65 kg / tree / year) [4, 6, 16].



In summary, this work aims the study of the phoenicicole biomass kinetics, under slow pyrolysis (10 °C / min), corresponding to DN cultivar, using the TGA. Two statistical analyses (analysis of variance and principal component analysis PCA) were used to allow the interpretation of the results. Thus, this study will enable us to answer and address the following research questions:

What is the thermal behavior of the phoenicicole biomass related to DN cultivar, under pyrolysis process? What are the kinetic (activation energy, order of the reaction, preexponential factor) and the thermal characteristics (onset and offset devolatilization temperature) of the phoenicicole biomass related to DN cultivar? What are the most interesting phoenicicole biomass constituents, related to DN cultivar, for pyrolysis process?

The area chosen for the realization of this study is the Guerrara oasis (Algeria - Latitude:  $32 \circ 47$  ' North Longitude:  $4 \circ 30$  East), which served as a model for the study of biomass deposit at the regional (Mzab) and national level (Algerian oasis) [4, 6, 16].

#### II. MATERIALS AND METHODS

A. Methods of sample preparation and chemical composition

Sampling, sample preparation and analysis (proximate, ultimate and calorimetry) were conducted according to the standards described in [6].

#### B. Thermogravimetric Analysis

The TGA is carried out in SETARAM Setsys Evolution 16/18 Thermogravimetric analyzer. The specification and test conditions of the Thermogravimetric analyzer are presented in Table I.

TABLE I.	SPECIFICATIONS AND TEST CONDITION OF
	THERMOGRAVIMETRIC ANALYZER

Model Balance sensitivity	Setsys Evolution 16-18 (model with integrated
	controller CS32)
Balance accuracy	0.4 µg
Maximum weight	200 mg
Temperature range	25 to 1600°C
Heating and cooling rates	0.1 – 200 °C/min in 0.1 increments
Type of sample	Solids, liquids, powders, films or fibers
TGA atmosphere	Static or dynamic including nitrogen, argon, carbon
	dioxide, air, oxygen or other inert or active gases
Temperature sensors	S type thermocouple with 10% rhodium platinum
Heating rate	10°C/min
Purge gas	N <sub>2</sub>
Purge gas rate	200 ml/min
Initial temperature of the	25.00 °C
sample	
Final temperature	600 °C

#### C. Kinetic parameters

Thermogravimetric analysis (TGA) leads to the thermal characterization (chemical kinetics) of the biomass by direct measurement of their mass as a function of the temperature and (or) time. This chemical kinetics of different thermochemical conversions (pyrolysis, combustion or gasification) combined with other parameters (chemistry) can provide the necessary information for the understanding and optimization of these processes [17]. Several additional techniques are used in parallel at the TGA for the determination of kinetic parameters (differential thermal analysis DTA ...).

Bibliographical references mention several studies and methods for the determination of kinetic parameters [9, 12, 15, 18-22]; that used for our case is based on the FRIEDMAN model [23]. All these kinetic models are based on the Arrhenius equation given by:

$$\frac{d\alpha}{dt=A \exp[(-E)/RT]} (1-\alpha)^n$$
(1)

Where:  $d\alpha/dt$ , A, n, E, R,  $\alpha$ , T, t are respectively the conversion rate, the pre-exponential(s<sup>-1</sup>), the order of reaction, activation energy (kJ/mol), the universal gas constant, the fraction of reactant decomposed at time t (%), the absolute temperature (°K) and the time (s).

#### Given that:

The mathematical form of the conversion  $\alpha$  can be written as :

$$u = (w_0 - w) / (w_0 - w_f)$$
<sup>(2)</sup>

• The constant heating rate  $\beta$ , is given by :

$$\beta = dT/dt$$
 (3)

Where: w,  $w_0$  and  $w_f$  are respectively the weight of the sample at a particular time t, its initial and final weight.

The equation (1) is written:

$$d\alpha/dT = A/\beta \exp[(-E)/RT](1-\alpha)^n$$
(4)

$$d\alpha / (1-\alpha)^{n} = A/\beta \exp[(-E)/RT] dT$$
(5)

Considering some approximations:

Rearrangement and integration of equation (5)

• Approximation of the order of the reaction to the unity

The equation (5) becomes:

$$\ln(1-\alpha) = A/\beta [(R.T^2)/E] \exp[(-E)/RT)]$$
 (6)

$$\ln[-\ln(1-\alpha)] = \ln[A/\beta.(R.T^{2})/E] - E/RT$$
(7)

This equation is of the form:

$$\mathbf{y} = \mathbf{b} + \mathbf{a}\mathbf{x} \tag{8}$$

Where:

 $y = \ln[-\ln(1-\alpha)]$ ;  $b = \ln[A/\beta.(R.T^2)/E$ ; a = -E/R; x = 1/T



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The constant a is estimated by simple linear regression data obtained from the TGA on the major interval devolatilization of the biomass studied. Microsoft Excel was used for these calculations. The results obtained, namely the activation energy E and  $R^2$  regression coefficient, are shown in Fig. 2 and Table II.

### D. Principal compnent Analysis PCA

The Principal Component Analysis (PCA) was applied to:

- Thermal parameters which includes: onset and offset devolatilization temperatures of pyrolysis (T<sub>onset</sub> and T<sub>offset</sub>), the corresponding activation energies, the yield (ΔMass) of the thermochemical process and the calorific value of biomass (HHV).
- Chemical parameters which includes: proximate parameters (fixed carbon FC, volatile matter VM and ashes A). The moisture parameter was not taken in account for the PCA because of its low variability.

### III. RESULTS AND DISCUSSION

#### A. Thermogravimetric analysis

Thermogravimetric analysis (TGA) of the date palm residues (DN cultivar case) performed under an inert atmosphere at 10°C/min, represents derivatives DTG mass depending on the temperature (Fig. 1). These curves show the main phases of the pyrolysis process related to the phoenicicole biomass and identify their thermal degradation profile:

- The first phase corresponds to the dehydration of the biomass i.e. the elimination of the moisture (between 100°C and 130°C) and the light volatiles matters (. It happens in a temperature range comprised between 31 and 198°C. Water is eliminated between 100°C and 130°C while light volatiles matters are extracted from 130°C to 250°C.
- The second phase is characterized by an important degradation of biomass. The second step of degradation is known as active pyrolysis zone where volatilization is at its maximum. In this stage, there is an intermolecular association and breaking chemical bonds. Due to the low temperatures, aliphatic side chains can break and small gas molecules form. Furthermore, the totality of volatiles is removed in this interval. It happens in a temperature that ranges between 198°C and 391°C on average. This phase also corresponds to the degradation of hemicellulose (250-350 °C) and cellulose (250-500 °C). For lignin this range is between 360-400 °C [24].

The **third phase** is characterized by the slow degradation of the remaining materials (char). In this interval (391°C and 600°C), the chemical bonds associated with higher temperatures can break and the compounds with high molecular weights are converted into small compounds molecular weight. This phase concerns essentially the degradation of lignin whose decomposition temperature is between 280°C and 450°C, and may exceed 500°C due to its thermal stability related to the phenolic hydroxyl group. The formation of a char characterizes the end of this phase [24].

Fig. 1 shows also the variation of the thermal behavior between biomass components translated by the variation of the temperature ranges. This can be explained essentially by the difference in the phoenicicole biomass composition especially on mineral level [6, 25, 26].



Figure 1. Typical dTG diagrams of the phoenicicole biomass related to the DN cultivar under inert atmosphere

#### B. Kinetic parameters

In order to simplify the interpretation and the exploitation of the thermograms, the interval considered for the calculation of the kinetic parameters is the one where the thermal decomposition process is the most important (maximum degradation rate). This calculation allowed to reach significant correlation coefficients  $R^2$  (Fig. 2 and Table II). Indeed, for pyrolysis process, this rate varies between 0.93 and 0.99, an average of 0.97.

Table II and Fig. 3 show the pyrolysis kinetic parameters (activation energy, reaction order and pre-exponential factor) of the phoenicicoles main residues related to Deglet Nour cultivar in the Guerrara oasis.

A general observation of the activation energy (Table II and Fig. 3) related to the phoenicicole main constituents (DN cultivar case) shows there is no significant variation of



2

0

-2

-4

-6

-8

1 0

-2

-3

-4

-5

2

In[-In(1-a)] 0

-1

-2

-3

2

0

-4

-6

-8

ହିଁ -2 In[-In(

y = -3,31x + 8 R<sup>2</sup> = 0,97 5.21

-3,90x + 6 R<sup>2</sup> = 0,98

-3,52x + 5,70 R<sup>2</sup> = 0,97

1/T

1/T

1/T

2

2

In[-In(1-a)] -1 y = -3,54x + 6,08 R<sup>2</sup> = 0,93

1/T

In[-In(1-a)]

AD

В

KН

SA

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TABLE II.



**Reaction order** 

n

1.18

1.47

0.68

0.65

0.70

0.58

0.81

SA

SA

KINETIC PARAMETERS OF PHOENICICOLE BIOMASS (DN

CULTIVAR CASE) UNDER INERT ATMOSPHERE

this parameter among different wastes. The average value is estimated at 28.78 kJ/mol (palm case). The energy d'activation varies between 26.71 kJ/mol (petiole case) and 32.46 kJ / mol (spathe case). On the basis of this parameter, we can say that the petiole (KER) appears slightly more advantageous than the remaining biomass study for pyrolysis process.



0.87 (SA) on average for the whole studied biomass. It varies between 0.58 (LIF) and 1.47 (ARJ). The pre-exponential factor varies very significantly

between 1.70 s<sup>-1</sup> and 648229.45 s<sup>-1</sup> for the pyrolysis process.

Figure 3. Kinetic parameters of phoenicicole biomass (DN Cultivar case) under inert atmosphere at 10°C/min

nicicole biomass constit

a : Activation Energy ; b : Ordre of the reaction ; c : pre-exponential factor



#### C. Classification of the main phoenicicole biomass

Four categories of the studied biomass were identified after the principal component analysis according to the settings mentioned above (see Fig. 4):

The **first group** represents the LIF sample of DN cultivar; it is characterized by high ash content (~ 16%), fixed carbon (~ 29%) and cellulose content (50.6%. This group is characterized by thermal stability mainly due to the high lignin content. This explains the high devolatilization temperatures (195.46 °C and 394.50 °C respectively), the low calorific value (15 MJ/kg) and low conversion rate (55%).

The inflorescence part (fruit stalk pruning (SA) and fruit bunch (ARJ) spathe (KH)) represents the **second group**. In contrast to the first group (on the plane symmetrical), the second is characterized by a high thermal reactivity explained by a high content of hemicellulose and a low ash (~ 8%). This explains the high calorific value (20 MJ/kg) and an elevated pyrolysis yield (70%). Moreover, the initial and final temperatures of devolatilization (153 – 376 °C) are relatively low in comparison to the previous group.

The **third group** represents the basal part of the palm (AD and KER) and the spathe (KH) corresponding to DN cultivar. This group is characterized by intermediate values for all parameters (energetic and chemical) with the exception of the activation energy and high heating value, which are respectively estimated on average at 29 kJ / mol and 19 MJ / kg and are relatively high compared with other samples.

The palms (DJ) constitute the **last group** (fourth) which is characterized by almost equivalent cellulose and hemicellulose content, very high ash content (~19%), a significant calorific value (20 MJ / kg). these elements explain a high pyrolysis yield (69%).



Figure 4. Projection of variables on the factor-plans (1 x 2)

#### IV. CONCLUSION

Thermogravimetric analysis TGA was carried out to study thermal behavior of the phoenicicole main constituents related to Deglet Nour cultivar considering pyrolysis process. The approach used is based on the calculation of the kinetic parameters (activation energy, reaction order and preexponential factor), the review of the different thermal characteristics related to the biomass decomposition phases and the classification of studied biomass taking into account energetic and chemical parameters.

The thermal profile of the phoenicicole biomass is characterized by three decomposition stages corresponding to: dehydration, degradation of hemicellulose and cellulose and finally degradation of lignin which behaves as a thermal stabilizer.

In spite of invariability for the pyrolysis activation energy among different phoenicicole constituents, four groups were identified on the basis of their thermal behavior and chemical composition. The two characteristics categories are: firstly, the Lif part is inappropriate to a thermal conversion in an inert atmosphere because of its thermal stability due to the high content of lignin and ash. Secondly, the inflorescence part which may favor such thermoconversion thanks to a high thermal reactivity of dominant constituent i.e. hemicellulose and the low ash content.

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